

Low-temperature catalytic oxidation of volatile organic compounds (VOC) mixture using wood fly ash (WFA) and oxygen

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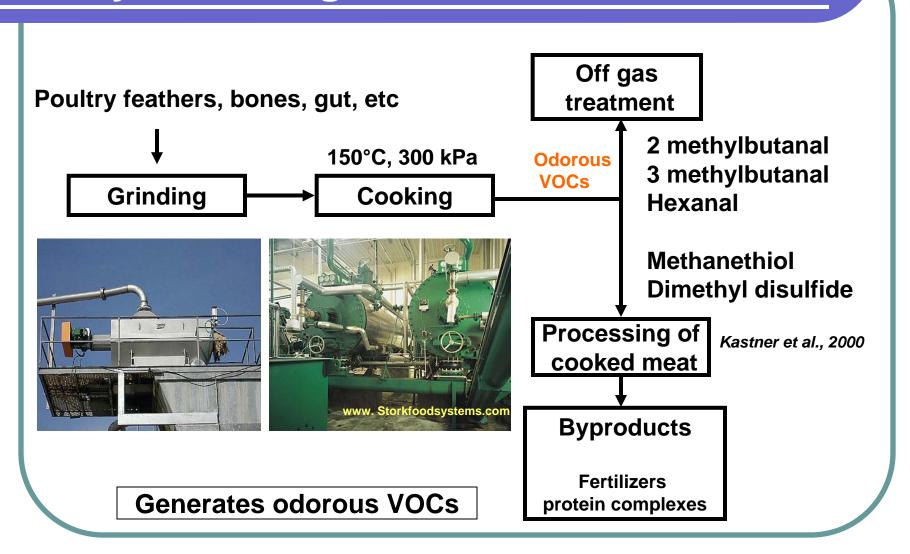
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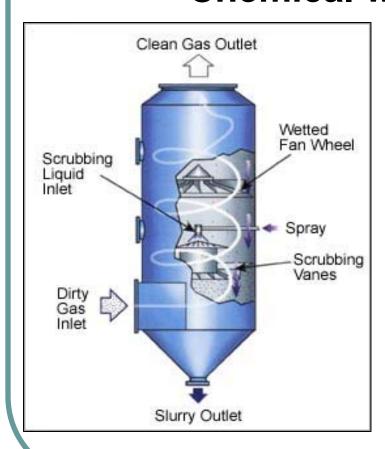


The goal is to treat air pollutants from poultry rendering emissions



Present treatment technology does not completely remove VOCs from rendering

Chemical wet scrubber



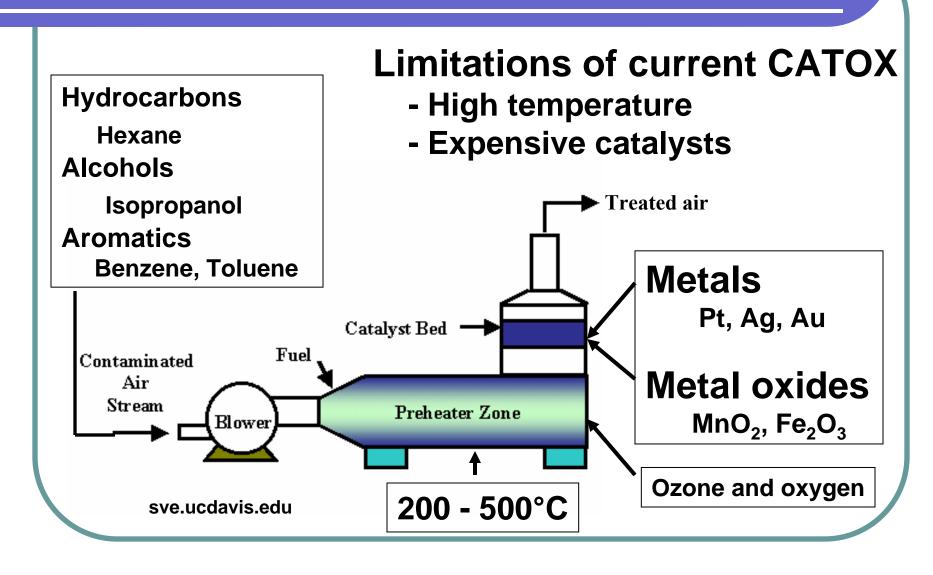
- Liquid phase oxidation
- CIO₂ and Ozone
- Water intensive
- Expensive chemicals
- Selective reaction

Sulfur based: good Aldehydes: no reaction

- Kastner et al., 2003

Need a more efficient technology

Catalytic oxidation (CATOX) has been used to treat several VOCs

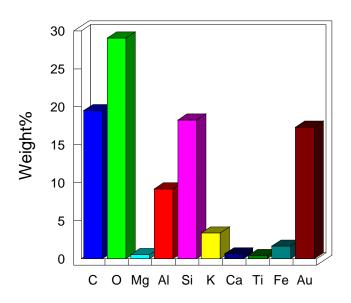


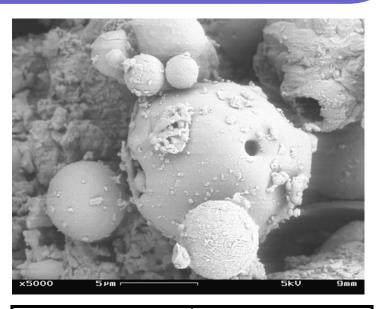
Analysis of wood fly ash via SEM and XRD revealed carbon and metals

What is wood fly ash?

- Ash from burning of wood
- 5.5 Million Tons/Yr
- Contains metals and carbon

Quantitative results





Density	0.54 g/cc
Area	$45 \pm 8 \text{ m}^2/\text{g}$
рН	12 ± 0.12

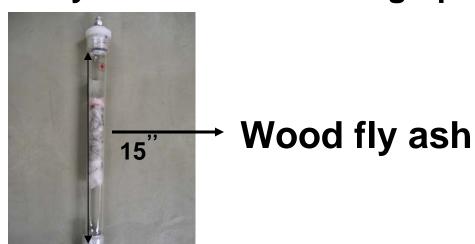
The objective was to test wood fly ash as a catalyst for oxidation of VOC mixture

Test compounds: 2 methylbutanal (2-MB) and hexanal

Approach: Test individually and as mixture

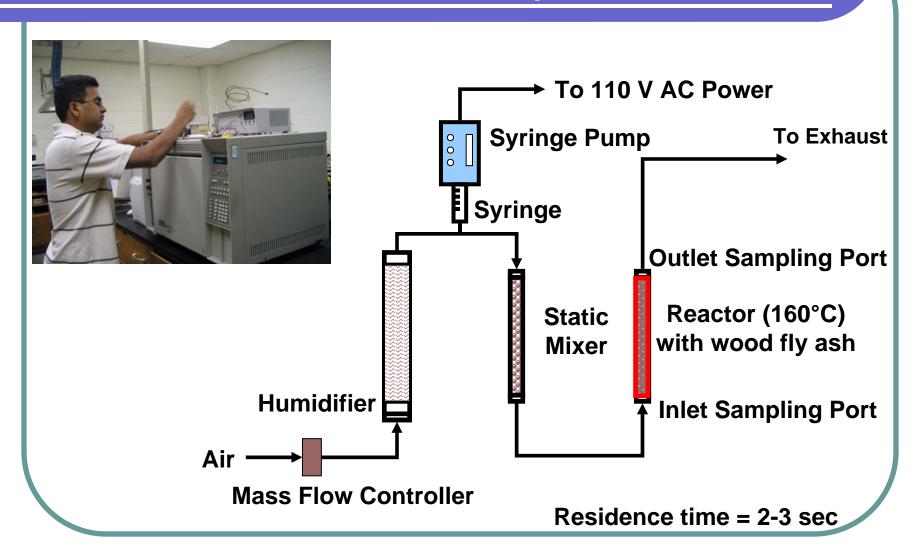
Experimental: 2 L/min, 400-600 ppmv inlet, 160°C

Analytical: Gas chromatograph with MS and FID



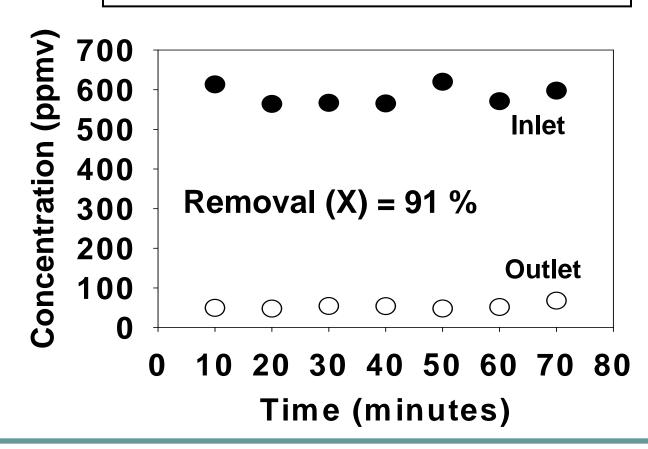


Removal was measured in a packed bed continuous flow reactor system

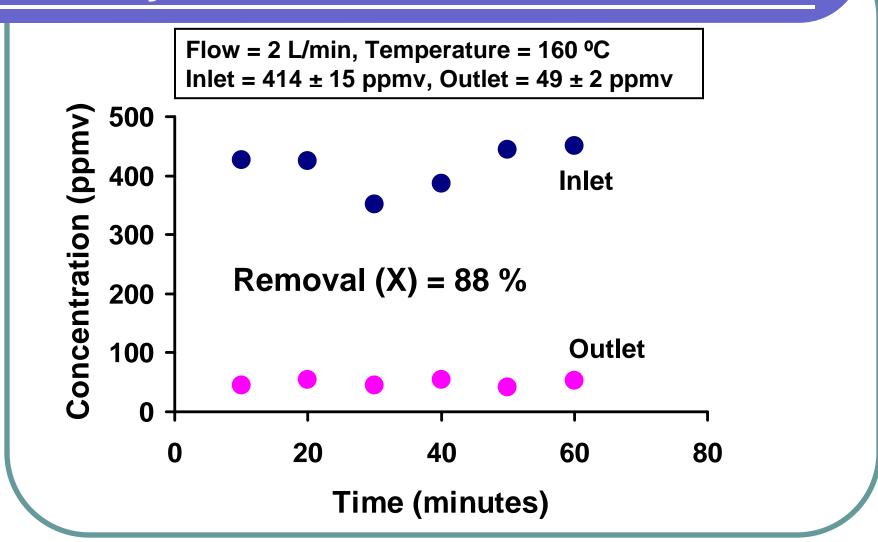


90 % of 2-methylbutanal was removed using wood fly ash

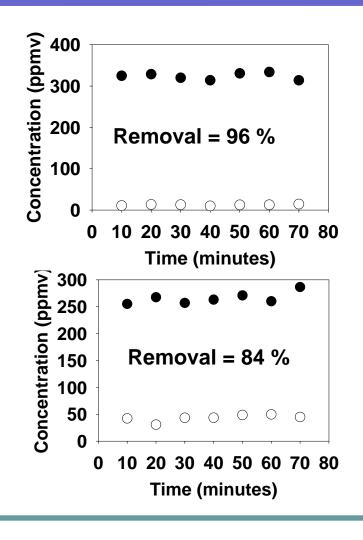
Flow = 2 L/min, Temperature = 160 °C Inlet = 583 ± 9 ppmv, Outlet = 53 ± 3 ppmv



88 % of hexanal was removed using wood fly ash



84-96 % of 2MB and hexanal mixture was removed



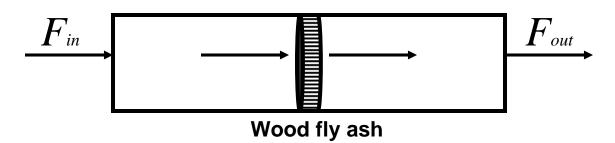
2 Methybutanal

Flow = 2 L/min Temperature = 160 °C Inlet (ppmv) = 324 ± 3 Outlet = 12 ± 0.6

Hexanal

Flow = 2 L/min Temperature = 160 °C Inlet (ppmv) = 266 ± 4 Removal (%) = 43 ± 2

A differential plug flow reactor model was used for determining oxidation rates



$$F_{in} - F_{out} + rW = \frac{dN}{dt}$$
 Mole balance equation

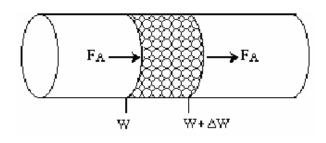
Assuming steady, isothermal, and isobaric conditions

$$-r = Q_0 \frac{P_T}{RT} y \frac{X}{W}$$
 Final equation $Q_0 = Flow \ rate, P_T = Total \ pressure$ $y = Mole \ fraction, \ X = \% \ Conversion$ $T = Temperature, \ R = Gas \ const$ $W = Catalyst \ mass$

Wood fly ash was comparable with other catalysts

Compound	Catalyst	Concentration (ppmv)	Temp (°C)	Reaction rates	Reference
2-methylbutanal hexanal	Wood fly ash	400-600	160	3.2 - 4.7	This work
Formaldehyde	MnOx- CeO ₂	580	60-100	5	Tang et al., 2006
Acetaldehyde	Pt/Rh	360 - 510	205	13 - 14	Liakopoulos et al., 2001
Hexane	Pt-Ni/γ- Al ₂ O	200-566	164-221	1-18	Gangwal et al., 1988

Based on the experimental data the reactor may be designed for 99 % removal



$$-r = \frac{dF}{dW}$$

$$W = Q \int_{C_{in}}^{C_{out}} \frac{dC_{in}}{k C_{in}^n}$$

$$\rho\left(\frac{V}{Q}\right) = \rho \tau = \int_{C_{in}}^{C_{out}} \frac{dC_{in}}{r}$$

In summary, wood fly ash may be used as a catalyst to treat aldehydes

Wood fly ash is catalytically active

- Oxygen can be used as an oxidant
- Can remove mixtures
- 90-99 % removal may be possible in 3-5 sec (at 160°C)

Acknowledgements

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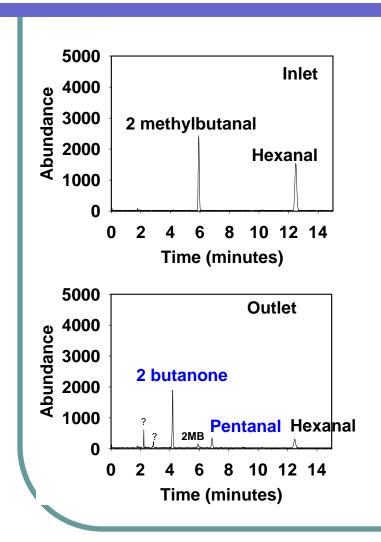


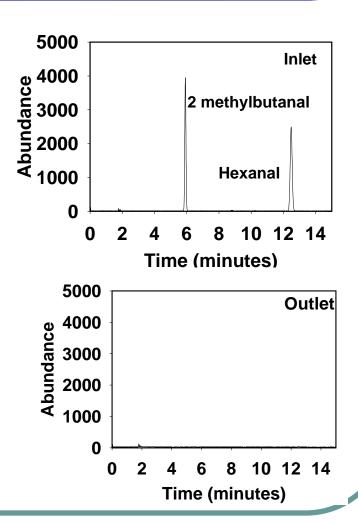




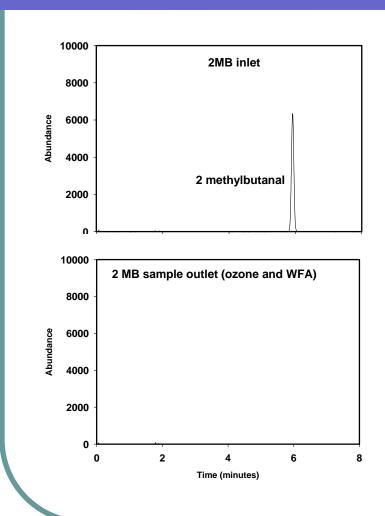


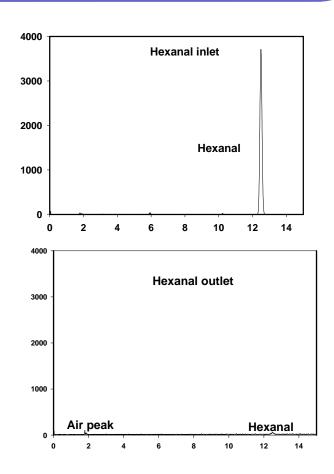
80-90 % of mixture was removed with oxygen and ozone and wood fly ash





Wood fly ash and ozone completely oxidized aldehydes (160 deg C, 2L/min flow, 10 g ash)



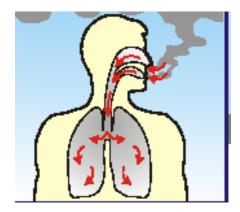


Volatile organic compounds (VOCs) are hazardous

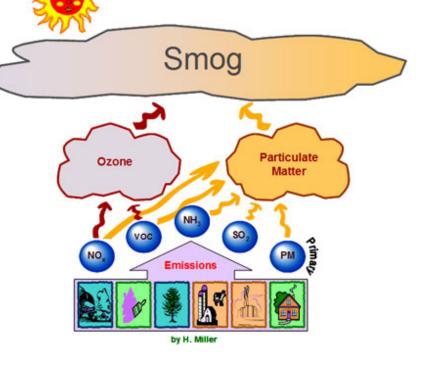
VOC: Any carbon-based chemical that participates in photochemical

reactions (USEPA 40 CFR Part 5)

Health: Short and long term



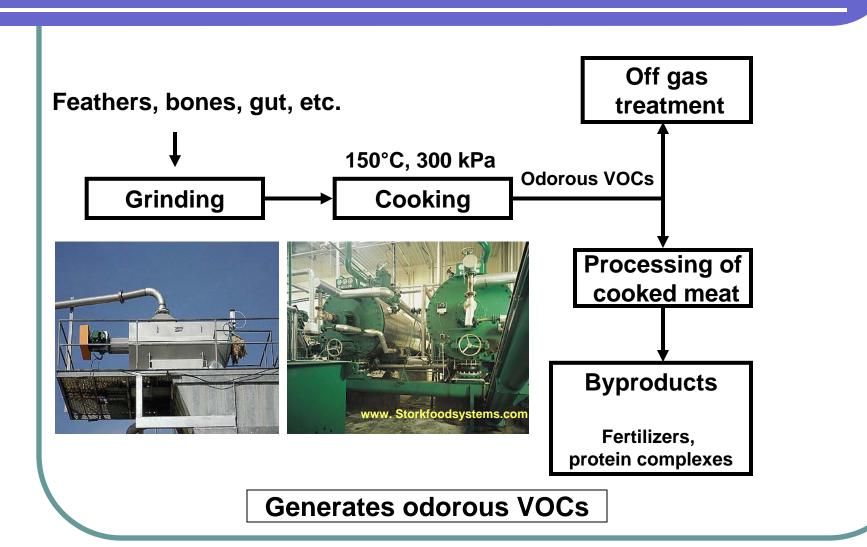
Environmental: Ozone, PM



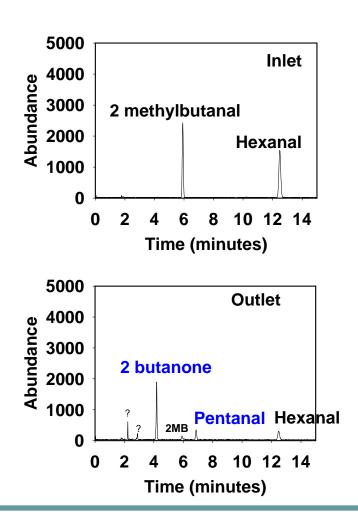
Environment Canada

VOCs are mostly manmade

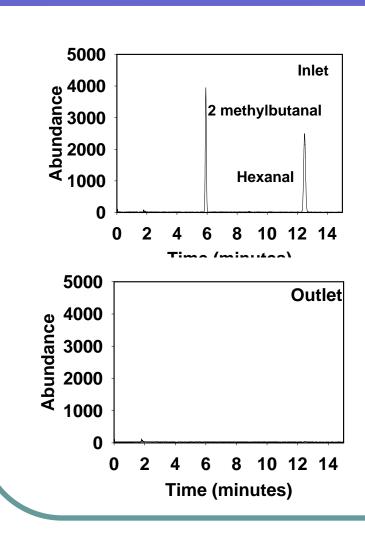
Poultry rendering generates odorous VOCs'



Oxygen and wood fly ash removed up to 90 % of mixture within 3 seconds



Ozone completely oxidized 2-MB and hexanal mixture within 3 seconds



100 % removal was obtained with ozone and wood fly ash

